

Esterification of Glycerol by Oleic Acid and Selective Hydrogenation of Oleic Acid Methyl ester Over Acid and Ru-Sn-B Supported Mesoporous AIMCM-41

Qiu Bin KAN^{1*}, J. BARRAULT², Tong Hao WU¹

¹Department of Chemistry, Jilin University, Changchun 130023

²Laboratoire de Catalyse, CNRS URA 350-ESIP, 40, 86022 Poitiers, Cedex, France

Abstract: The AIMCM-41 molecular sieves with two different pore sizes are hydrothermally synthesized in the presence of surfactants with two different chain lengths. H-AIMCM-41 and Ru-Sn-B/H-AIMCM-41 which are prepared by the conventional ion-exchange and incipient wetness techniques of the AIMCM-41 show fair catalytic activity for esterification of glycerol by oleic acid and selective hydrogenation of oleic acid methyl ester, respectively.

Keywords: AIMCM-41, Ru-Sn-B/H-AIMCM-41, oleic acid, esterification, hydrogenation.

Demand for large pore size molecular sieves has given rise to great interests in a new family of silica-based mesoporous materials designated as M41s, which expand typical molecular sieves into an extra-large pore range and generate the potential for the applications of these materials in catalysis and sorption for very bulky molecules¹⁻⁶. MCM-41 possesses a hexagonal arrangement of uniform mesopore ranging from 15 to 100 Å and can be prepared with varied Si/Al ratios. The investigations of the materials with very large uniform pore and acidic property have opened new possibilities for processing and producing large molecules. Esterification of glycerol by oleic acid and selective hydrogenation of unsaturated fatty ester for obtaining unsaturated alcohol are two important reactions of fine chemicals^{7,8}. The acid AIMCM-41 with larger pore size is considered advantageous as catalyst or catalytic support for the two reactions. This note reports the preparations of acid AIMCM-41 and Pt-Sn-B supported AIMCM-41 catalysts and their catalytic performances for the two selected reactions.

Preparation of H-AIMCM-41 and Ru-Sn-B/H-AIMCM-41

AIMCM-41 material with Si/Al=40 is synthesized from a reaction mixture SiO₂-H₂O-TMAOH-C_nTMACl-NaOH-NaAlO₂ (or pseudoboehmite) (n=12 or 16)^{1-3,9}. A typical example of preparation is as follows: solution A is obtained by addition of Cab-O-Sil M5 and NaOH to water. Mixing of another Cab-O-Sil M5 and TMAOH•5H₂O with water forms solution B. Solution C contains C₁₆TMACl (25%) and water. At first the solution A is combined with the solution B, and then the solution C is dropped with

* E-mail: qkan@mail.jlu.edu.cn

vigorous stirring into the mixture, followed by addition of a certain amount of Cab-O-Sil M5 and sodium aluminate or pseudoboehmite. Since sodium aluminate may introduce extraneous cations into the reaction mixture interfering the synthesis, sodium ions in solution A are quantitatively deducted on the basis of the amount of sodium aluminate, if it is used as aluminum source in the preparation. The resulting reaction mixture (pH \approx 11.5) is placed in Teflon-lined stainless steel autoclaves, sealed and shaken before heating to 110°C. After 24-72 hours, the autoclaves are cooled to room temperature and the solid products are filtered and washed with distilled water, and then dried at 100°C for 6 hours. The as-synthesized samples are calcined in a stream of nitrogen from room temperature to 550°C at a rate of 1°C/min, followed by calcination in air at 550°C for 6 hours. The calcined AIMCM-41 samples are ion-exchanged in 1.2 mol/L of NH₄NO₃ solution with liquid to solid ratio of 15 mL/g in order to form NH₄-AIMCM-41. The H-form of AIMCM-41 is obtained by heating the NH₄-AIMCM-41 at 600°C in air. The preparation procedure of Ru-Sn-B/MCM-41 is as follows: 0.1685 g of RuCl₃·xH₂O and 0.6239 g of SnCl₂·H₂O are firstly mixed in a flask, and then 3.0 g of H-AIMCM-41 is impregnated with the aqueous solution. This paste is left to stand for 20 hours. 0.3377 g of NaBH₄ is dissolved in 8.5 g of water and added to the above slurry of the impregnated H-AIMCM-41. After the reduction is completed, the solid is washed with distilled water and absolute alcohol, respectively, dried in the flow of N₂ at 120°C, and then treated by H₂ at 400°C for 12 hours before using as catalysts.

Characterization of mesoporous samples

XRD measurements reveal that the as-synthesized and calcined mesoporous samples have MCM-41 structures. When quaternary ammonium surfactant C_nTMACl with n=12 and 16 are respectively used as templates, the mesoporous AIMCM-41 materials exhibiting different d-spacing are obtained. The surfactant chain length has effect on the d-spacing (or pore size (2)) of the AIMCM-41: the longer the surfactant chain is, the larger the d-spacing is. The calcined AIMCM-41 is sensitive to treatment in water even at room temperature. Putting AIMCM-41C₁₆ (synthesized using C₁₆ TMACl as template) into water for 6 hours, the first peak intensity of its XRD patterns dramatically decreases. However, after calcination at 550°C, the peak intensity is almost recovered. Similar phenomenon is observed in the NH₄⁺-exchange experiment of AIMCM-41C₁₆. The H-AIMCM-41 formed upon calcination of NH₄-MCM-41 has X-ray diffraction patterns similar to the calcined AIMCM-41. Chemical analysis shows that there is small difference of Si/Al ratio between reaction gels and the mesoporous products. The surface area of AIMCM-41C₁₂ (synthesized using C₁₂TMACl as template) is similar to that of AIMCM-41C₁₆ (~900m²/g). For AIMCM-C₁₂, the H-form has somewhat larger surface area than the calcined sample. In contrast, for AIMCM-41C₁₆, aqueous solution can partly reduce its crystallinity causing a decrease in the surface area after NH₄⁺ exchange to produce H-AIMCM-41C₁₆ by calcination. The surface area of Ru-Sn-B/H-AIMCM-41C₁₆ (~460m²/g) is smaller than that of H-AIMCM-41C₁₆ (~755m²/g) because of introduction of guest atoms into the channel occupying the

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surface. The total amount of acid sites determined by NH_3 -TPD and titration methods is 0.75 and 0.58 mmol/g for H-AIMCM-41C₁₆ and H-AIMCM-41C₁₂, respectively.

Catalytic reactions

Esterification of glycerol by oleic acid over H-AIMCM-41

The catalytic reaction is carried out under normal pressure. The catalytic reaction results are listed in **Table 1**. H-AIMCM-41 catalysts are active for esterification of glycerol by oleic acid. However, H-AIMCM-41C₁₆ and H-AIMCM-41C₁₂ show different activity for producing ester of glycerol. Clearly H-AIMCM-41C₁₆ which should have larger pore diameter than H-AIMCM-41C₁₂ is more active than H-AIMCM-41C₁₂. On the other hand, H-AIMCM-41C₁₂ is more efficient in confining the larger volume of products, such as trioleate of glycerol and monooleate of diglycerol. Selectivity of product with smaller volume (monooleate of glycerol) obviously increases when using H-AIMCM-41C₁₂ instead of H-AIMCM-41C₁₆ as catalysts. In comparison with the size of the esterification products of glycerol by oleic acid, the pore size of H-AIMCM-41C₁₂ may be still too large for an effective shape-selectivity of monooleate of glycerol. It is therefore expected that a further smaller pore of AIMCM-41 would be more selective for obtaining monooleate of glycerol.

Table 1 Esterification of glycerol by oleic acid

Catalyst	Yield (%) Ester of glycerol	Distribution of some ester products (%)			
		MG	DG	TG	MD
H-MCM-41C ₁₆	45	31	7	2	60
H-MCM-41C ₁₂	22	61	10	1	28

MG=monooleate of glycerol, DG=diolate of glycerol, TG=trioleate of glycerol, MD=monooleate of diglycerol

Selective hydrogenation of oleic acid methyl ester over Ru-B-Sn/H-AIMCM-41

The hydrogenation reaction is carried out under the pressure of 80 bar (H_2 50%, N_2 50%) at 270-280°C, using 1.1 g of catalyst and 50 mL of reactant oleic acid methyl ester. **Table 2** gives the results of catalytic hydrogenation reactions of oleic acid methyl ester over Ru-B-Sn/H-MCM-41C₁₆ and shows that the supported mesoporous catalyst is effective for selective hydrogenation of unsaturated fatty ester to form unsaturated alcohol. It is observed that both conversion of hydrogenation and selectivity to unsaturated alcohol is increased with the reaction time. On the other hand, heavy ester decreases with the reaction time. At a longer reaction time, such as 21 hours, saturated alcohol and ester can be tested.

As a conclusion, H-AIMCM-41 and Ru-Sn-B/H-AIMCM-41 catalysts are potential for esterification of glycerol by oleic acid and selective hydrogenation of oleic acid methyl ester. Further investigations should be done in order to obtain optimal reaction conditions and better catalytic performance and to fairly understand catalytic mechanism.

Table 2 Selective hydrogenation of oleic acid methylester over Ru-B-Sn/H-AIMCM-41C₁₆

Time (h)	Conversion (%)	Selectivity (%)				Hydrogenolysis Products
		Unsaturated Alcohol	Saturated Alcohol	Heavy Ester	Saturated Ester	
1	19.5	3.0	--	76.5	--	20.5
3	30.5	9.5	--	54.5	--	36.0
4	47.5	21.5	--	63.0	--	15.5
6	62.5	46.0	--	42.0	--	12.0
8	74.5	47.5	--	41.0	--	11.5
21	90.5	53.5	3	20.5	6	17.0

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